



RAILROAD COMMISSION OF TEXAS

Form G-1

1701 N. Congress  
P.O. Box 12967  
Austin, Texas 78701-2967

Status: Approved  
Date: 03/15/2018  
Tracking No.: 181945

GAS WELL BACK PRESSURE TEST, COMPLETION OR RECOMPLETION REPORT, AND LOG

OPERATOR INFORMATION	
Operator Name: ELEVATION RESOURCES LLC	Operator No.: 247756
Operator Address: 200 N LORAIN STE 1010 MIDLAND, TX 79701-0000	

WELL INFORMATION	
API No.: 42-003-47118	County: ANDREWS
Well No.: 5H	RRC District No.: 08
Lease Name: UNIVERSITY 1-26 UNIT	Field Name: EMMA (DEVONIAN)
RRC Gas ID No.: 283482	Field No.: 28899166
Location: Section: 26, Block: 1, Survey: UL, Abstract: U26	
Latitude:	Longitude:
This well is located 10 miles in a SOUTH-SOUTHEASTERLY direction from ANDREWS, TEXAS, which is the nearest town in the county.	

FILING INFORMATION		
Purpose of filing: Reclass Oil to Gas		
Type of completion: Other/Recompletion		
Well Type: Producing	Completion or Recompletion Date: 01/15/2017	
Type of Permit	Date	Permit No.
Permit to Drill, Plug Back, or Deepen	04/24/2015	805597
Rule 37 Exception		
Fluid Injection Permit		
O&G Waste Disposal Permit		
Other:		

COMPLETION INFORMATION			
Spud date: 07/04/2016	Date of first production after rig released: 01/15/2017		
Date plug back, deepening, recompletion, or drilling operation commenced: 07/04/2016	Date plug back, deepening, recompletion, or drilling operation ended: 11/27/2016		
Number of producing wells on this lease in this field (reservoir) including this well: 3	Distance to nearest well in lease & reservoir (ft.): 1226.0		
Total number of acres in lease: 728.22	Elevation (ft.): 3145 GL		
Total depth TVD (ft.): 11117	Total depth MD (ft.): 17770		
Plug back depth TVD (ft.):	Plug back depth MD (ft.):		
Was directional survey made other than inclination (Form W-12)? Yes	Rotation time within surface casing (hours): 108.0		
Recompletion or reclass? Yes	Is Cementing Affidavit (Form W-15) attached? Yes		
Type(s) of electric or other log(s) run: Gamma Ray (MWD)	Multiple completion? No		
Electric Log Other Description:			
Location of well, relative to nearest lease boundaries of lease on which this well is located:	Off Lease: No		
	500.0 Feet from the North Line and		
	400.0 Feet from the West Line of the		
	UNIVERSITY 1-26 UNIT Lease.		

FORMER FIELD (WITH RESERVOIR) & GAS ID OR OIL LEASE NO.			
Field & Reservoir	Gas ID or Oil Lease No.	Well No.	Prior Service Type

G1:	N/A				
PACKET	EMMA (DEVONIAN)	47300	5H	Producing	
FOR NEW DRILL OR RE-ENTRY, SURFACE CASING DEPTH DETERMINED BY:					
GAU Groundwater Protection Determination		Depth (ft.): 1575.0	Date: 03/27/2015		
SWR 13 Exception		Depth (ft.):			

GAS MEASUREMENT DATA										
Date of test: 05/18/2017					Gas measurement method(s):					
Gas production during test (MCF): 4107					Orifice Meter					
Was the well preflowed for 48 hours? Yes										
Run No.	Line size	Orif. or Choke Size (in.)	24 hr. Coeff. Orif. Or Choke (in.)	Static Pm or Choke (in.)	Diff (hw)	Flow Temp (°F)	Temp. (Ftf)	Gravity (Fg)	Compress (Fpv)	Volume (MCF/day)
1	3.000	1.5	12.39	65.0	143.0	89.0	1.3000	0.7980	1.008	1369.0

FIELD DATA AND PRESSURE CALCULATIONS										
Gravity (dry gas): 0.798					Gravity (liquid hydrocarbons) (Deg. API): 49.4					
Gas-Liquid Hydro Ratio (CF/Bbl): 4373					Gravity (mixture): Gmix= 1.345					
Avg. shut in temp. (°F): 89.0					Bottom hole temp. and depth: 165.0 °F@ 11117.0 FT					
Run No.	Time of Run (Min.)	Choke Size (in.)	Wellhead Pressure (PSIA)		Wellhead Flow Temp (°F )					
SHUT-IN	720	64/64	300		93.0					
1	4320	64/64	150		90.0					

CASING RECORD										
Row	Type of Casing	Casing Size (in.)	Hole Size (in.)	Setting Depth (ft.)	Multi - Stage Depth (ft.)	Multi - Shoe Cement Class	Cement Amount (sacks)	Slurry Volume (cu. ft.)	Top of Cement (ft.)	TOC Determined By
1	Surface	13 3/8	17 1/2	1629		CLASS "C"	1460	2708.2	0	Circulated to Surface
2	Intermediate	9 5/8	12 1/4	7121		TRANSTE X MULTI	2600	5744.0	3112	Calculation
3	Intermediate	9 5/8	12 1/4	7121	3112	TRANSTE X MULTI C	1400	2840.0	0	Calculation
4	Intermediate	7	8 3/4	11399		TRANSTE X MULTI	900	1942.0	6910	Calculation
5	Intermediate	7	8 3/4	11399	6910	TRANSTE X MULTI	700	1458.0	0	Circulated to Surface

LINER RECORD									
Row	Liner Size (in.)	Hole Size (in.)	Liner Top (ft.)	Liner Bottom (ft.)	Cement Class	Cement Amount (sacks)	Slurry Volume (cu. ft.)	Top of Cement (ft.)	TOC Determined By
1	4 1/2	6 1/8	10254	17753	ULTRA "C"	550	946.0	10254	Calculation

TUBING RECORD			
Row	Size (in.)	Depth	Packer Depth (ft.)/Type
1	2 7/8	9900	/

PRODUCING/INJECTION/DISPOSAL INTERVAL			
Row	Open hole?	From (ft.)	To (ft.)
1	No	L1 11450	17704

ACID, FRACTURE, CEMENT SQUEEZE, CAST IRON BRIDGE PLUG, RETAINER, ETC.			
Was hydraulic fracturing treatment performed?		Yes	
Is well equipped with a downhole actuation sleeve?		No	
		If yes, actuation pressure (PSIG):	
Production casing test pressure (PSIG) prior to hydraulic fracturing treatment:		8500	
		Actual maximum pressure (PSIG) during hydraulic fracturing:	
		8269	
Has the hydraulic fracturing fluid disclosure been reported to FracFocus disclosure registry (SWR29)?		Yes	
Row	Type of Operation	Amount and Kind of Material Used	Depth Interval (ft.)
1	Fracture	PLEASE SEE FRAC FOCUS FOR DETAILS	11450.0 17704.0
2	Other	520 SX CMT PLUG SET IN 8-3/4" WELLBORE	7284.0 7500.0
3	Other	520 SX CMT PLUG SET IN 8-3/4" WELLBORE	6152.0 7278.0

FORMATION RECORD						
Formations	Encountered	Depth TVD (ft.)	Depth MD (ft.)	Is formation isolated?	Remarks	
YATES	Yes	3157.0	3157.0	Yes	ESTIMATED - NOT LOGGED	
SEVEN RIVERS	Yes	3271.0	3271.0	Yes	ESTIMATED - NOT LOGGED	
QUEEN	Yes	3380.0	3380.0	Yes	ESTIMATED - NOT LOGGED	
GRAYBURG	Yes	4750.0	4750.0	Yes	ESTIMATED - NOT LOGGED	
SAN ANDRES - CO2 FLOOD, HIGH FLOWS, H2S, CORROSIVE	Yes	4915.0	4915.0	Yes	ESTIMATED - NOT LOGGED	
HOLT	No			No	NOT GEOLOGICALLY PRESENT	
GLORIETA	Yes	5720.0	5720.0	Yes	ESTIMATED - NOT LOGGED	
TUBB	No			No	NOT GEOLOGICALLY PRESENT	
CLEARFORK	Yes	6715.0	6715.0	Yes	ESTIMATED - NOT LOGGED	
PERMIAN DETRITAL	No			No	NOT GEOLOGICALLY PRESENT	
LEON	No			No	NOT GEOLOGICALLY PRESENT	
WICHITA ALBANY	Yes	7830.0	7830.0	Yes	ESTIMATED - NOT LOGGED	
SPRABERRY	No			No	NOT GEOLOGICALLY PRESENT	
DEAN	No			No	NOT GEOLOGICALLY PRESENT	
WOLFCAMP	Yes	8557.0	8557.0	Yes	ESTIMATED TOP - NO LOG	
CANYON	No			No	NOT GEOLOGICALLY PRESENT	
PENNSYLVANIAN	Yes	8780.0	8780.0	Yes		
MCKEE	No			No	WELL NOT DRILLED DEEP ENOUGH	
STRAWN	Yes	9736.0	9736.0	Yes		
FUSSELMAN	No			No	WELL NOT DRILLED DEEP ENOUGH	

DEVONIAN	Yes	11023.0	11023.0	Yes
SILURIAN	No			No WELL NOT DRILLED DEEP ENOUGH
ELLENBURGER	No			No WELL NOT DRILLED DEEP ENOUGH

Do the producing interval of this well produce H2S with a concentration in excess of 100 ppm (SWR 36)? No

Is the completion being downhole commingled (SWR 10)? No

REMARKS
KOP @ 10,650'

RRC REMARKS
<p><b>PUBLIC COMMENTS:</b></p> <p>[RRC Staff 2017-11-08 11:38:20.069] EDL=6254 feet, max acres=260</p> <p><b>CASING RECORD :</b></p> <p><b>TUBING RECORD:</b></p> <p><b>PRODUCING/INJECTION/DISPOSAL INTERVAL :</b></p> <p><b>ACID, FRACTURE, CEMENT SQUEEZE, CAST IRON BRIDGE PLUG, RETAINER, ETC. :</b></p> <p>FISH STUCK IN HOLE, ON 7/23/16 2 CMT PLUGS WERE SET TO ABANDON WELLBORE AND CEMENT OFF WATER FLOW. RE-ENTERED 11/2/16 TO FINISH DRILLING. PLUGS WERE LEFT IN PLACE, JUST SIDETRACKED AROUND TO CONTINUE</p> <p><b>GAS MEASUREMENT DATE REMARK:</b></p>

OPERATOR'S CERTIFICATION	
<b>Printed Name:</b> Curtis Flanagan	<b>Title:</b> Eng. Tech
<b>Telephone No.:</b> (432) 688-3380	<b>Date Certified:</b> 02/13/2018

RAILROAD COMMISSION OF TEXAS  
Oil and Gas DivisionGAS WELL  
CLASSIFICATION REPORT

Form G-5

Tracking No.: 181945

This facsimile G-5 was generated electronically from data submitted to the RRC.

1. OPERATOR NAME (Exactly as shown on Form P5 Organization Report) <b>ELEVATION RESOURCES LLC</b>		3. RRC DISTRICT NO. <b>08</b>	4. OIL LEASE NO OR GAS WELL ID NO. <b>283482</b>																																																				
2. MAILING ADDRESS <b>200 N LORAIN STE 1010 MIDLAND, TX 79701</b>		5. WELL NO. <b>5H</b>	6. API NO. <b>42- 003-47118</b>																																																				
		7. COUNTY OF WELL SITE <b>ANDREWS</b>																																																					
8. FIELD NAME (as per RRC Records) <b>EMMA (DEVONIAN)</b>		9. LEASE NAME <b>UNIVERSITY 1-26 UNIT</b>																																																					
10. LOCATION (Section, Block and Survey) <b>26 , 1 , UL , A-U26</b>		11. PIPELINE CONNECTION OR USE OF GAS <b>JAMES LAKE MIDSTREAM LLC (429665)</b>																																																					
<b>PRODUCTION TEST AT RATE ELECTED BY OPERATOR</b> (data on 24-hour basis)		<b>A.S.T.M. DISTILLATION OF LIQUID SAMPLE.</b> Distillation test is required for gas wells ONLY if the producing gas-liquid hydrocarbon ratio is less than 100,000 CF/barrel.																																																					
<table><tr><td>A. Date of Test</td><td><u>05/18/2017</u></td></tr><tr><td>B. Gas Volume</td><td><u>1369.0</u> (Mcf)</td></tr><tr><td>C. Oil or Condensate Volume</td><td><u>313.0</u> (Bbl)</td></tr><tr><td>D. Water Volume</td><td><u>1381.0</u> (Bbl)</td></tr><tr><td>E. Gas/Liquid Hydrocarbon Ratio</td><td><u>4373</u> (Cf/Bbl)</td></tr><tr><td>F. Flowing Tubing Pressure</td><td><u>150</u> (psia)</td></tr><tr><td>G. Choke Size</td><td><u>64/64</u> (in.)</td></tr><tr><td>H. Casing Pressure</td><td><u>180.0</u> (psia)</td></tr><tr><td>I. Shut-in Wellhead Pressure-- Tubing</td><td><u>300</u> (psia)</td></tr><tr><td>J. Separator Operating Pressure</td><td><u>65.0</u> (psia)</td></tr><tr><td>K. Color of Stock Tank Liquid</td><td><u>Dark Straw</u></td></tr><tr><td>L. Gravity of Separator Liquid</td><td><u>44.6</u> °API</td></tr><tr><td>M. Gravity of Stock Tank Liquid</td><td><u>45.0</u> °API</td></tr><tr><td>N. Specific Gravity of the Gas (Air = 1)</td><td><u>0.798</u></td></tr></table>		A. Date of Test	<u>05/18/2017</u>	B. Gas Volume	<u>1369.0</u> (Mcf)	C. Oil or Condensate Volume	<u>313.0</u> (Bbl)	D. Water Volume	<u>1381.0</u> (Bbl)	E. Gas/Liquid Hydrocarbon Ratio	<u>4373</u> (Cf/Bbl)	F. Flowing Tubing Pressure	<u>150</u> (psia)	G. Choke Size	<u>64/64</u> (in.)	H. Casing Pressure	<u>180.0</u> (psia)	I. Shut-in Wellhead Pressure-- Tubing	<u>300</u> (psia)	J. Separator Operating Pressure	<u>65.0</u> (psia)	K. Color of Stock Tank Liquid	<u>Dark Straw</u>	L. Gravity of Separator Liquid	<u>44.6</u> °API	M. Gravity of Stock Tank Liquid	<u>45.0</u> °API	N. Specific Gravity of the Gas (Air = 1)	<u>0.798</u>	<table><tr><td colspan="2">Date Liquid Sample Obtained <u>09/13/2017</u></td></tr><tr><td>Where Obtained:</td><td><input checked="" type="checkbox"/> Separator <input type="checkbox"/> Stock Tank</td></tr><tr><td>% Over Temp. (deg. F)</td><td>% Over Temp. (deg. F)</td></tr><tr><td>Initial Boiling Temp. <u>94.0</u></td><td>60 <u>543.0</u></td></tr><tr><td>10 <u>205.0</u></td><td>70 <u>637.0</u></td></tr><tr><td>20 <u>256.0</u></td><td>80 <u>721.0</u></td></tr><tr><td>30 <u>309.0</u></td><td>90 _____</td></tr><tr><td>40 <u>377.0</u></td><td>95 _____</td></tr><tr><td>50 <u>462.0</u></td><td>End Point <u>726.0</u></td></tr><tr><td>Total Recovery</td><td><u>81.9</u> percent</td></tr><tr><td>Residue</td><td><u>16.3</u> percent</td></tr><tr><td>Loss</td><td><u>1.8</u> percent</td></tr></table>		Date Liquid Sample Obtained <u>09/13/2017</u>		Where Obtained:	<input checked="" type="checkbox"/> Separator <input type="checkbox"/> Stock Tank	% Over Temp. (deg. F)	% Over Temp. (deg. F)	Initial Boiling Temp. <u>94.0</u>	60 <u>543.0</u>	10 <u>205.0</u>	70 <u>637.0</u>	20 <u>256.0</u>	80 <u>721.0</u>	30 <u>309.0</u>	90 _____	40 <u>377.0</u>	95 _____	50 <u>462.0</u>	End Point <u>726.0</u>	Total Recovery	<u>81.9</u> percent	Residue	<u>16.3</u> percent	Loss	<u>1.8</u> percent
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<p>I declare under penalties prescribed in Sec. 91.143, Texas Natural Resources Code, that I am authorized to make this report, that this report was prepared by me or under my supervision and direction, and that data and facts stated therein are true, correct, and complete to the best of my knowledge.</p> <p><u>11/08/2017</u> DATE</p>		<b>RRC USE ONLY</b>																																																					
				<u>ELEVATION RESOURCES LLC</u>																																																			
				NAME (Type or Print)																																																			
				<u>Curtis Flanagan</u> SIGNATURE																																																			
<u>Eng. Tech</u> TITLE																																																							
<u>(432) 688-3380</u> CONTACT PERSON		PHONE NUMBER																																																					

Tracking No.: 181945

OPERATOR NAME AND ADDRESS including city, state and zip

ELEVATION RESOURCES LLC

200 N LORAIN STE 1010  
MIDLAND, TX 79701**GAS WELL  
STATUS REPORT**RAILROAD COMMISSION OF TEXAS  
Oil and Gas Division  
P.O. Box 12967  
Austin, Texas 78711-2967*This facsimile G-10 was generated electronically  
from data submitted to the RRC.*

Reason for Filing

☐

Survey

☐

Retest

☒

Initial Test

☐

Correction

Operator P-5 Organization No.

247756

RRC Dist. No.

08

**G-10**

Test Period:

Due Date:

Effective Date:

FIELD NAME * LEASE NAME	RRC IDENT NO.	DATE TESTED MO/DAY/YR	GAS PRODUCED MCF/DAY **	CONDENSATE PRODUCED	WATER PROD BBL/DAY	***SIWH PRESSURE PSIA
	WELL NO.	MARK X FOR SHUT-IN WELL	GAS SPEC. GRAVITY	CONDENSATE GRAVITY (API)	X BOTTOMHOLE PRESSURE PSIA	***FLOWING PRESSURE PSIA
EMMA (DEVONIAN)	283482	05/18/2017	1369 MCF	313.0 BBL	1381.0 BBL	300
UNIVERSITY 1-26 UNIT	5H		0.798	49.4		150
			MCF	BBL	BBL	
			MCF	BBL	BBL	
			MCF	BBL	BBL	
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			MCF	BBL	BBL	
			MCF	BBL	BBL	
			MCF	BBL	BBL	
			MCF	BBL	BBL	

CERTIFICATION: I declare under penalties prescribed in Texas Natural Resources Code, Sec. 91.143, that I am authorized to make this report, that this report was prepared by me or under my supervision and direction, and that data and facts stated herein are true, correct, and complete to the best of my knowledge.

ELEVATION RESOURCES LLC

Signature: LEONARD STICKEL

Title:

Phone: (432)686-7500

Date: 11/08/2017

\* AN ASTERISK PREPRINTED ON A SURVEY IDENTIFIES WELL SUBJECT TO COMMINGLING TEST REQUIREMENT

\*\* GAS PRODUCTION RATE, IN MCF, IS TO BE REPORTED FULL-Well STREAM, INCLUDING  
CONDENSATE \*\*\* PRESSURE FOR THE TEXAS HUGOTON FIELD IS REPORTED IN PSIG

X AN 'X' PREPRINTED ON A SURVEY IN THE BOTTOMHOLE PRESSURE BOX INDICATES A BOTTOMHOLE PRESSURE MUST BE REPORTED FOR THE WELL

**Retrograde Gas PVT Fluid Study  
for  
Elevation Resources LLC  
University 1-26 Unit No. 5H  
Andrews County, Texas**

The analysis, opinions and interpretations contained in this report are based upon observations, assumptions, empirical factors, inferences and data supplied by the customer, which are not infallible. The results expressed in this report represent the best judgment of FESCO. Accordingly, FESCO assumes no responsibility and makes no warranty as to the accuracy or correctness of any analysis, opinion or interpretation. FESCO shall not be liable or responsible for any loss, cost, damage, claim or expense whatsoever incurred or sustained by the customer resulting from any analysis, opinion or interpretation made by any of our employees.



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## FESCO, Ltd.

Petroleum Engineers

Petroleum Engineers

CORPORATE HEADQUARTERS: 1000 FESCO AVE. • ALICE, TEXAS 78332-7318 • (361) 661-7000

ALICE.....(361) 664-3479	BRYAN.....(979) 775-1825	EL CAMPO.....(979) 543-9451	ODESSA.....(432) 332-3211
ALICE LAB.....(361) 661-7015	CORPUS CHRISTI	HOUSTON SALES (281) 565-1115	OZONA.....(325) 392-3773
ALICE HYDRAULICS (361) 661-1538	PROD. TESTING...(361) 882-4124	KILGORE.....(903) 984-4814	PECOS.....(432) 445-1993
BEAUMONT.....(409) 842-3000	WIRELINE.....(361) 452-1631	LAREDO.....(956) 724-7501	REFUGIO.....(361) 526-4644
BRIDGEPORT, WV....(304) 592-3366	EDINBURG.....(956) 383-8378	LUFKIN.....(936) 632-7036	VICTORIA.....(361) 575-7533

September 26, 2017

Mr. Mark Solari  
Elevation Resources LLC  
200 N. Loraine, Suite 1010  
Midland, Texas 79701

Re: Well: University 1-26 Unit No. 5H  
Field: Emma (Devonian)  
Location: Andrews County, Texas  
Formation: Devonian  
Lateral: 11450 - 17704 ft MD  
Test Type: Retrograde Gas PVT Fluid Study

Dear Mr. Solari:

The attached report contains results from a laboratory study performed on the recombined separator fluids from the subject well. The study determined the type and character of the reservoir fluid. The fluid study was performed using first-stage separator gas and hydrocarbon (HC) liquid samples obtained from the well on September 13, 2017 by FESCO, Ltd. FESCO then delivered the separator samples to its PVT laboratory in Alice, Texas. Extended compositional analyses were performed on the separator gas (C<sub>11+</sub>) and on the separator HC liquid (C<sub>31+</sub>) samples. Tables 1-A through 1-D list the compositional analyses of the separator gas, separator HC liquid and mathematically recombined wellstream fluid through C<sub>7+</sub>, C<sub>11+</sub> and C<sub>31+</sub>, respectively. The Appendix contains the ASTM D-86 distillation conducted on the stock tank HC liquid. Table 2 reports the fluid properties measured as the separator HC liquid was flashed from separator conditions to ambient laboratory conditions.

The separator gas and HC liquid were physically recombined in a visual PVT cell at the reservoir temperature of 165 °F and at the reported gas-oil ratio of 8628 Scf/Sep Bbl (8981 Scf/STB). The recombined fluid was evaluated during a Constant Composition Expansion (CCE) process at pressures ranging from 9015 to 1103 psia. The resulting CCE data is reported in Table 3. *A retrograde dew point was observed at 8420 psia.* The static reservoir pressure is lower than the observed retrograde dew point pressure. Therefore, the reservoir fluid exists as saturated (two-phase)

Elevation Resources LLC  
University 1-26 Unit No. 5H  
September 26, 2017

gas at static reservoir conditions of 4815 psia and 165 °F. Figures 1 through 7 illustrate the data reported in Table 3.

Thank you for this opportunity to serve Elevation Resources LLC. Please call me if you have any questions or concerns regarding this report.

Sincerely,

FESCO, Ltd.



Raj K. Lahoti, E.I.T.  
Petroleum Engineer  
Alice, Texas  
Phone: 361-661-7015  
Email: [raj.lahoti@fescoinc.com](mailto:raj.lahoti@fescoinc.com)



Bobby Mandel, P. E.  
Vice - President  
Alice, Texas  
Phone: 361-661-7000 Ext. 141  
Email: [bobby.mandel@fescoinc.com](mailto:bobby.mandel@fescoinc.com)

**FESCO, Ltd.***Petroleum Engineers***SAMPLE SUMMARY**

Company:	Elevation Resources LLC
Well:	University 1-26 Unit No. 5H
Sample Date:	09/13/17
Sample Time:	9:15 AM

**Separator Conditions**

Pressure:	110 psia
Temperature:	88 °F

**Laboratory Quality Test**

Separator Gas:	<u>Pressure</u>	<u>Temperature</u>
Cylinder ID No. G-3512P*	120 psia	130 °F
Cylinder ID No. G-3519	119 psia	130 °F
Separator HC Liquid:	<u>BP Pressure</u>	<u>Temperature</u>
Cylinder ID No. W-2873*	100 psia	70 °F
Cylinder ID No. W-1518	100 psia	70 °F

Report Date: 9/26/2017

\* Samples used in fluid study

## TABLE 1-A

### COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, HC LIQUID AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C<sub>7+</sub>

HC LIQUID AND GAS CYLINDERS.....: W-2873\* and G-3512P\*

SEPARATOR GLR.....: 8628 Scf/Sep Bbl

SEPARATOR PRESSURE.....: 110 psia

SEPARATOR TEMPERATURE.....: 88 °F

STL TOTAL SAMPLE SG .....: 0.7821 (Water = 1.000)

Component	SEPARATOR GAS			SEPARATOR HC LIQUID			WELLSTREAM			COMP. PROPERTIES	
	Weight %	Mole%	* GPM	Weight %	Mole %	Liquid Volume %	Weight %	Mole %	GPM	MW lb/lb-mole	SG H2O=1.000
Hydrogen Sulfide	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	34.081	0.7989
Nitrogen	1.332	1.094	0.000	0.004	0.023	0.004	0.877	1.016	0.000	28.013	0.8069
Carbon Dioxide	1.522	0.796	0.000	0.019	0.065	0.018	1.006	0.743	0.000	44.010	0.8172
Methane	49.652	71.217	0.000	0.255	2.437	0.665	32.707	66.218	0.000	16.043	0.3000
Ethane	19.282	14.755	3.924	0.574	2.926	1.260	12.865	13.896	3.695	30.069	0.3563
Propane	13.660	7.128	1.953	1.344	4.670	2.072	9.435	6.949	1.904	44.096	0.5072
Iso-butane	1.877	0.743	0.242	0.406	1.070	0.564	1.372	0.767	0.250	58.122	0.5628
N-butane	5.802	2.297	0.720	1.843	4.861	2.468	4.444	2.483	0.778	58.122	0.5842
2-2 Dimethylpropane	0.016	0.005	0.002	0.039	0.083	0.051	0.024	0.011	0.004	72.149	0.5967
Iso-pentane	1.536	0.490	0.178	1.161	2.465	1.452	1.407	0.633	0.230	72.149	0.6251
N-pentane	2.038	0.650	0.234	2.060	4.377	2.555	2.046	0.921	0.332	72.149	0.6307
2-2 Dimethylbutane	0.015	0.004	0.002	0.020	0.036	0.024	0.017	0.006	0.003	86.177	0.6540
Cyclopentane	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	70.135	0.7504
2-3 Dimethylbutane	0.146	0.039	0.016	0.207	0.369	0.243	0.167	0.063	0.026	86.177	0.6664
2 Methylpentane	0.446	0.119	0.049	0.850	1.511	1.010	0.584	0.220	0.091	86.177	0.6579
3 Methylpentane	0.240	0.064	0.026	0.514	0.914	0.601	0.334	0.126	0.051	86.177	0.6689
Other Hexanes	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	84.000	0.6850
n-Hexane	0.712	0.190	0.078	1.838	3.270	2.165	1.098	0.414	0.169	86.175	0.6641
Heptanes Plus	1.724	0.408	0.170	88.866	70.923	84.847	31.616	5.534	3.966	See Below	
TOTAL	100.000	100.000	7.593	100.000	100.000	100.000	100.000	100.000	11.499	---	---

HEPTANES PLUS (C <sub>7+</sub> ) FRACTION CHARACTERISTICS					
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole	Vapor Volume Scf/Gal	Gross Heating Value ***
	°API	**			
Separator Gas	N/A	3.3569	97.225	24.030	5,090
Separator HC Liquid	41.232	0.8192	192.053	13.537	131,390
Wellstream	N/A	0.8159	185.569	13.954	N/A

TOTAL SAMPLE CHARACTERISTICS						
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole	Vapor Volume Scf/Gal	GHV	
	°API	**			Dry ***	Saturated ***
Separator Gas	N/A	0.7980	23.010	131.700	1,348	1,325
Separator HC Liquid	49.413	0.7821	153.275	16.195	N/A	126,787
Wellstream	N/A	1.1214	32.479	86.968	N/A	N/A

\* GPM (gallons per Mscf) determined at 14.65 psia and 60°F

\*\* Gas specific gravity determined relative to air (SG=1.000).  
HC Liquid and wellstream specific gravity determined relative to water (SG=1.000).  
SG values determined mathematically using the compositional analysis.

\*\*\* Gross Heating Value units for gas (real basis) and HC liquid are BTU/Scf and BTU/Gal, respectively.

**TABLE 1-B**

**COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, HC LIQUID  
AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C<sub>11+</sub>**

HC LIQUID AND GAS CYLINDERS.....: W-2873\* and G-3512P\*  
SEPARATOR GLR.....: 8628 Scf/Sep Bbl  
SEPARATOR PRESSURE.....: 110 psia  
SEPARATOR TEMPERATURE.....: 88 °F  
STL TOTAL SAMPLE SG .....: 0.7821 (Water = 1.000)

Component	SEPARATOR GAS			SEPARATOR HC LIQUID			WELLSTREAM			COMP. PROPERTIES	
	Weight %	Mole%	* GPM	Weight %	Mole %	Liquid Volume %	Weight %	Mole %	GPM	MW lb/lb-mole	SG H20=1.000
Hydrogen Sulfide	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	34.081	0.7989
Nitrogen	1.332	1.094	0.000	0.004	0.023	0.004	0.877	1.016	0.000	28.013	0.8069
Carbon Dioxide	1.522	0.796	0.000	0.019	0.065	0.018	1.006	0.743	0.000	44.010	0.8172
Methane	49.652	71.217	0.000	0.255	2.437	0.665	32.707	66.218	0.000	16.043	0.3000
Ethane	19.282	14.755	3.924	0.574	2.926	1.260	12.865	13.896	3.695	30.069	0.3563
Propane	13.660	7.128	1.953	1.344	4.670	2.072	9.435	6.949	1.904	44.096	0.5072
Iso-butane	1.877	0.743	0.242	0.406	1.070	0.564	1.372	0.767	0.250	58.122	0.5628
N-butane	5.802	2.297	0.720	1.843	4.861	2.468	4.444	2.483	0.778	58.122	0.5842
2-2 Dimethylpropane	0.016	0.005	0.002	0.039	0.083	0.051	0.024	0.011	0.004	72.149	0.5967
Iso-pentane	1.536	0.490	0.178	1.161	2.465	1.452	1.407	0.633	0.230	72.149	0.6251
N-pentane	2.038	0.650	0.234	2.060	4.377	2.555	2.046	0.921	0.332	72.149	0.6307
2-2 Dimethylbutane	0.015	0.004	0.002	0.020	0.036	0.024	0.017	0.006	0.003	86.177	0.6540
Cyclopentanes	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	70.135	0.7504
2-3 Dimethylbutane	0.146	0.039	0.016	0.207	0.369	0.243	0.167	0.063	0.026	86.177	0.6664
2 Methylpentane	0.446	0.119	0.049	0.850	1.511	1.010	0.584	0.220	0.091	86.177	0.6579
3 Methylpentane	0.240	0.064	0.026	0.514	0.914	0.601	0.334	0.126	0.051	86.177	0.6689
Other Hexanes	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	84.000	0.6850
n-Hexane	0.712	0.190	0.078	1.838	3.270	2.165	1.098	0.414	0.169	86.175	0.6641
Methylcyclopentane	0.234	0.064	0.023	0.826	1.504	0.857	0.437	0.169	0.059	84.162	0.7536
Benzene	0.034	0.010	0.003	0.116	0.227	0.102	0.062	0.026	0.007	78.114	0.8844
Cyclohexane	0.161	0.044	0.015	0.705	1.284	0.704	0.348	0.134	0.045	84.162	0.7834
2-Methylhexane	0.100	0.023	0.011	0.664	1.015	0.760	0.293	0.095	0.044	100.205	0.6830
3-Methylhexane	0.113	0.026	0.012	0.627	0.959	0.709	0.289	0.094	0.043	100.205	0.6917
2,2,4 Trimethylpentane	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	114.232	0.6962
Other Heptanes	0.241	0.056	0.025	1.176	1.817	1.292	0.562	0.184	0.081	99.197	0.7122
n-Heptane	0.248	0.057	0.026	1.924	2.942	2.186	0.823	0.267	0.122	100.202	0.6882
Methylcyclohexane	0.192	0.045	0.018	1.697	2.649	1.715	0.708	0.234	0.094	98.189	0.7740
Toluene	0.044	0.011	0.004	0.542	0.901	0.486	0.215	0.076	0.025	92.143	0.8718
Other C8's	0.187	0.039	0.018	3.641	5.063	3.875	1.372	0.404	0.191	110.217	0.7349
n-Octane	0.065	0.013	0.007	1.743	2.338	1.929	0.640	0.182	0.093	114.229	0.7066
Ethylbenzene	0.005	0.001	0.000	0.154	0.222	0.138	0.056	0.017	0.007	106.168	0.8718
M&P-Xylene	0.023	0.005	0.002	0.733	1.058	0.661	0.266	0.082	0.031	106.168	0.8670
O-Xylene	0.005	0.001	0.000	0.334	0.482	0.295	0.118	0.036	0.014	106.168	0.8848
Other C-9's	0.055	0.010	0.005	3.268	3.967	3.391	1.157	0.298	0.157	126.243	0.7536
n-Nonane	0.011	0.002	0.001	1.564	1.869	1.694	0.544	0.138	0.077	128.255	0.7222
Other C10's	0.006	0.001	0.001	4.071	4.416	4.149	1.400	0.322	0.187	141.278	0.7675
n-Decane	0.000	0.000	0.000	1.203	1.296	1.281	0.413	0.094	0.057	142.282	0.7346
Undecanes Plus	0.000	0.000	0.000	63.881	36.912	58.624	21.913	2.683	2.631	See Below	
TOTAL	100.000	100.000	7.593	100.000	100.000	100.0000	100.000	100.000	11.499	N/A	N/A

UNDECANES PLUS (C <sub>11+</sub> ) FRACTION CHARACTERISTICS					
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole	Vapor Volume Scf/Gal	Gross Heating Value *** ****
	°API	**			
Separator Gas	N/A	0.8523	265.300	10.196	8,400
Separator HC Liquid	34.524	0.8523	265.265	10.197	133,468
Wellstream	N/A	0.8523	265.265	10.197	N/A

TOTAL SAMPLE CHARACTERISTICS						
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole	Vapor Volume Scf/Gal	GHV	
	°API	**			Dry	Saturated
					***	***
Separator Gas	N/A	0.7980	23.010	131.700	1,348	1325
Separator HC Liquid	49.413	0.7821	153.275	16.195	N/A	126,787
Wellstream	N/A	1.1214	32.479	86.968	N/A	N/A

\* GPM (gallons per Mscf) determined at 14.65 psia and 60°F

\*\* Gas specific gravity determined relative to air (SG=1.000).  
HC Liquid and wellstream specific gravity determined relative to water (SG=1.000).  
SG values determined mathematically using the compositional analysis.

\*\*\* Gross Heating Value units for gas (real basis) and HC liquid are BTU/Scf and BTU/Gal, respectively.

## TABLE 1-C

### COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, HC LIQUID AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C<sub>31+</sub>

HC LIQUID AND GAS CYLINDERS.....: W-2873\* and G-3512P\*

SEPARATOR GLR.....: 8628 Scf/Sep Bbl

SEPARATOR PRESSURE.....: 110 psia

SEPARATOR TEMPERATURE.....: 88 °F

STL TOTAL SAMPLE SG .....: 0.7821 (Water = 1.000)

Component	SEPARATOR GAS			SEPARATOR HC LIQUID			WELLSTREAM			COMP. PROPERTIES	
	Weight %	Mole%	* GPM	Weight %	Mole %	Liquid Volume %	Weight %	Mole %	GPM	MW lb/lb-mole	SG H2O=1.000
Hydrogen Sulfide	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	34.081	0.7989
Nitrogen	1.332	1.094	0.000	0.004	0.023	0.004	0.877	1.016	0.000	28.013	0.8069
Carbon Dioxide	1.522	0.796	0.000	0.019	0.065	0.018	1.006	0.743	0.000	44.010	0.8172
Methane	49.652	71.217	0.000	0.255	2.437	0.665	32.707	66.218	0.000	16.043	0.3000
Ethane	19.282	14.755	3.924	0.574	2.926	1.260	12.865	13.896	3.695	30.069	0.3563
Propane	13.660	7.128	1.953	1.344	4.670	2.072	9.435	6.949	1.904	44.096	0.5072
Iso-butane	1.877	0.743	0.242	0.406	1.070	0.564	1.372	0.767	0.250	58.122	0.5628
N-butane	5.802	2.297	0.720	1.843	4.861	2.468	4.444	2.483	0.778	58.122	0.5842
2-2 Dimethylpropane	0.016	0.005	0.002	0.039	0.083	0.051	0.024	0.011	0.004	72.149	0.5967
Iso-pentane	1.536	0.490	0.178	1.161	2.465	1.452	1.407	0.633	0.230	72.149	0.6251
N-pentane	2.038	0.650	0.234	2.060	4.377	2.555	2.046	0.921	0.332	72.149	0.6307
2-2 Dimethylbutane	0.015	0.004	0.002	0.020	0.036	0.024	0.017	0.006	0.003	86.177	0.6540
Cyclopentanes	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	70.135	0.7504
2-3 Dimethylbutane	0.146	0.039	0.016	0.207	0.369	0.243	0.167	0.063	0.026	86.177	0.6664
2 Methylpentane	0.446	0.119	0.049	0.850	1.511	1.010	0.584	0.220	0.091	86.177	0.6579
3 Methylpentane	0.240	0.064	0.026	0.514	0.914	0.601	0.334	0.126	0.051	86.177	0.6689
Other Hexanes	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	84.000	0.6850
n-Hexane	0.712	0.190	0.078	1.838	3.270	2.165	1.098	0.414	0.169	86.175	0.6641
Methylcyclopentane	0.234	0.064	0.023	0.826	1.504	0.857	0.437	0.169	0.059	84.162	0.7536
Benzene	0.034	0.010	0.003	0.116	0.227	0.102	0.062	0.026	0.007	78.114	0.8844
Cyclohexane	0.161	0.044	0.015	0.705	1.284	0.704	0.348	0.134	0.045	84.162	0.7834
2-Methylhexane	0.100	0.023	0.011	0.664	1.015	0.760	0.293	0.095	0.044	100.205	0.6830
3-Methylhexane	0.113	0.026	0.012	0.627	0.959	0.709	0.289	0.094	0.043	100.205	0.6917
2,2,4 Trimethylpentane	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	114.232	0.6962
Other Heptanes	0.241	0.056	0.025	1.176	1.817	1.292	0.562	0.184	0.081	99.197	0.7122
n-Heptane	0.248	0.057	0.026	1.924	2.942	2.186	0.823	0.267	0.122	100.202	0.6882
Methylcyclohexane	0.192	0.045	0.018	1.697	2.649	1.715	0.708	0.234	0.094	98.189	0.7740
Toluene	0.044	0.011	0.004	0.542	0.901	0.486	0.215	0.076	0.025	92.143	0.8718
Other C8's	0.187	0.039	0.018	3.641	5.063	3.875	1.372	0.404	0.191	110.217	0.7349
n-Octane	0.065	0.013	0.007	1.743	2.338	1.929	0.640	0.182	0.093	114.229	0.7066
Ethylbenzene	0.005	0.001	0.000	0.154	0.222	0.138	0.056	0.017	0.007	106.168	0.8718
M&P-Xylene	0.023	0.005	0.002	0.733	1.058	0.661	0.266	0.082	0.031	106.168	0.8670
O-Xylene	0.005	0.001	0.000	0.334	0.482	0.295	0.118	0.036	0.014	106.168	0.8848
Other C-9's	0.055	0.010	0.005	3.268	3.967	3.391	1.157	0.298	0.157	126.243	0.7536
n-Nonane	0.011	0.002	0.001	1.564	1.869	1.694	0.544	0.138	0.077	128.255	0.7222
Other C10's	0.006	0.001	0.001	4.071	4.416	4.149	1.400	0.322	0.187	141.278	0.7675
n-Decane	0.000	0.000	0.000	1.203	1.296	1.281	0.413	0.094	0.057	142.282	0.7346
Undecanes	0.000	0.000	0.000	4.521	4.714	4.543	1.551	0.343	0.204	147.000	0.7783
Dodecanes	0.000	0.000	0.000	3.974	3.783	3.939	1.363	0.275	0.177	161.000	0.7892
Tridecanes	0.000	0.000	0.000	4.070	3.564	3.979	1.396	0.259	0.179	175.000	0.8000
Tetradecanes	0.000	0.000	0.000	3.620	2.920	3.492	1.242	0.212	0.157	190.000	0.8109
Pentadecanes	0.000	0.000	0.000	3.319	2.470	3.163	1.139	0.180	0.142	206.000	0.8207
Hexadecanes	0.000	0.000	0.000	3.054	2.108	2.886	1.047	0.153	0.130	222.000	0.8276
Heptadecanes	0.000	0.000	0.000	2.712	1.754	2.539	0.930	0.128	0.114	237.000	0.8355
Octadecanes	0.000	0.000	0.000	2.678	1.636	2.493	0.919	0.119	0.112	251.000	0.8404
Nonadecanes	0.000	0.000	0.000	2.631	1.533	2.434	0.903	0.111	0.109	263.000	0.8454
Eicosanes	0.000	0.000	0.000	2.348	1.309	2.160	0.805	0.095	0.097	275.000	0.8503
Heneicosanes	0.000	0.000	0.000	1.939	1.021	1.773	0.665	0.074	0.080	291.000	0.8552
Docosanes	0.000	0.000	0.000	1.908	0.959	1.735	0.654	0.070	0.078	305.000	0.8602
Tricosanes	0.000	0.000	0.000	1.860	0.897	1.682	0.638	0.065	0.075	318.000	0.8651
Tetracosanes	0.000	0.000	0.000	1.675	0.776	1.508	0.575	0.056	0.068	331.000	0.8691
Pentacosanes	0.000	0.000	0.000	1.582	0.703	1.417	0.543	0.051	0.064	345.000	0.8730
Hexacosanes	0.000	0.000	0.000	1.253	0.535	1.117	0.430	0.039	0.050	359.000	0.8769
Heptacosanes	0.000	0.000	0.000	1.481	0.607	1.315	0.508	0.044	0.059	374.000	0.8809
Octacosanes	0.000	0.000	0.000	1.312	0.518	1.161	0.450	0.038	0.052	388.000	0.8839

**TABLE 1-C**

**COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, HC LIQUID  
AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C<sub>31+</sub>**

HC LIQUID AND GAS CYLINDERS.....: W-2873\* and G-3512P\*

SEPARATOR GLR.....: 8628 Scf/Sep Bbl

SEPARATOR PRESSURE.....: 110 psia

SEPARATOR TEMPERATURE.....: 88 °F

STL TOTAL SAMPLE SG .....: 0.7821 (Water = 1.000)

Component	SEPARATOR GAS			SEPARATOR HC LIQUID			WELLSTREAM			COMP. PROPERTIES	
	Weight %	Mole%	* GPM	Weight %	Mole %	Liquid Volume %	Weight %	Mole %	GPM	MW lb/lb-mole	SG H2O=1.000
Nonacosanes	0.000	0.000	0.000	1.244	0.474	1.097	0.427	0.034	0.049	402.000	0.8868
Triacosanes	0.000	0.000	0.000	1.029	0.379	0.904	0.353	0.028	0.041	416.000	0.8898
Hentriacontanes Plus	0.000	0.000	0.000	15.672	4.251	13.287	5.376	0.309	0.596	565.000	0.9225
TOTALS	100.000	100.000	7.593	100.000	100.000	100.000	100.000	100.000	11.499	N/A	N/A

HENTRIACONTANES PLUS (C <sub>31+</sub> ) FRACTION CHARACTERISTICS			
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole
	°API	**	
Separator Gas	N/A	N/A	N/A
Separator HC Liquid	21.888	0.9225	565.000
Wellstream	21.888	0.9225	565.000

TOTAL SAMPLE CHARACTERISTICS						
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole	Vapor Volume Scf/Gal	GHV	
	°API	**			Dry ***	Saturated ***
Separator Gas	N/A	0.7980	23.010	131.700	1,348	1325
Separator HC Liquid	49.413	0.7821	153.275	16.195	N/A	126,787
Wellstream	N/A	1.1214	32.479	86.968	N/A	N/A

\* GPM (gallons per Mscf) determined at 14.65 psia and 60°F

\*\* Gas specific gravity determined relative to air (SG=1.000).  
HC Liquid and wellstream specific gravity determined relative to water (SG=1.000).  
SG values determined mathematically using the compositional analysis.

\*\*\* Gross Heating Value units for gas (real basis) and HC liquid are BTU/Scf and BTU/Gal, respectively.

**TABLE 1-D**

**COMPOSITIONAL SCN ANALYSIS OF THE SEPARATOR GAS, HC LIQUID  
AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C<sub>31+</sub>**

HC LIQUID AND GAS CYLINDERS.....: W-2873\* and G-3512P\*  
SEPARATOR GLR.....: 8628 Scf/Sep Bbl  
SEPARATOR PRESSURE.....: 110 psia  
SEPARATOR TEMPERATURE.....: 88 °F  
STL TOTAL SAMPLE SG .....: 0.7821 (Water = 1.000)

Component	SEPARATOR GAS			SEPARATOR HC LIQUID			WELLSTREAM			COMP. PROPERTIES	
	Weight %	Mole%	* GPM	Weight %	Mole %	Liquid Volume %	Weight %	Mole %	GPM	MW lb/lb-mole	SG H2O=1.000
Hydrogen Sulfide	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	34.081	0.7989
Nitrogen	1.332	1.094	0.000	0.004	0.023	0.004	0.879	1.016	0.000	28.013	0.8069
Carbon Dioxide	1.522	0.796	0.000	0.019	0.065	0.018	1.009	0.743	0.000	44.010	0.8172
Methane	49.658	71.217	0.000	0.257	2.437	0.676	32.793	66.218	0.000	16.043	0.3000
Ethane	19.284	14.755	3.924	0.578	2.926	1.280	12.898	13.896	3.695	30.069	0.3563
Propane	13.662	7.128	1.953	1.354	4.670	2.105	9.460	6.949	1.904	44.096	0.5072
Iso-Butane	1.877	0.743	0.242	0.409	1.070	0.573	1.376	0.767	0.250	58.122	0.5628
n-Butane	5.803	2.297	0.720	1.857	4.861	2.507	4.456	2.483	0.778	58.122	0.5842
Iso-Pentanes	1.552	0.495	0.184	1.208	2.548	1.560	1.435	0.644	0.240	72.149	0.6109
n-Pentane	2.038	0.650	0.234	2.076	4.377	2.596	2.051	0.921	0.332	72.149	0.6307
Hexanes	1.559	0.416	0.171	3.455	6.100	4.115	2.206	0.829	0.340	86.177	0.6623
Heptanes	1.123	0.280	0.110	5.915	9.749	6.285	2.759	0.968	0.379	92.321	0.7424
Octanes	0.487	0.108	0.046	7.464	10.952	7.628	2.869	0.896	0.379	103.694	0.7718
Nonanes	0.095	0.019	0.008	5.724	7.599	5.506	2.017	0.570	0.251	114.600	0.8199
Decanes	0.006	0.001	0.001	5.323	5.712	5.590	1.821	0.416	0.248	141.780	0.7510
Undecanes	0.000	0.000	0.000	4.555	4.714	4.616	1.555	0.343	0.204	147.000	0.7783
Dodecanes	0.000	0.000	0.000	4.004	3.783	4.001	1.367	0.275	0.177	161.000	0.7892
Tridecanes	0.000	0.000	0.000	4.100	3.564	4.042	1.400	0.259	0.179	175.000	0.8000
Tetradecanes	0.000	0.000	0.000	3.647	2.920	3.547	1.245	0.212	0.157	190.000	0.8109
Pentadecanes	0.000	0.000	0.000	3.344	2.470	3.214	1.142	0.180	0.142	206.000	0.8207
Hexadecanes	0.000	0.000	0.000	3.076	2.108	2.932	1.050	0.153	0.130	222.000	0.8276
Heptadecanes	0.000	0.000	0.000	2.733	1.754	2.580	0.933	0.128	0.114	237.000	0.8355
Octadecanes	0.000	0.000	0.000	2.698	1.636	2.532	0.921	0.119	0.112	251.000	0.8404
Nonadecanes	0.000	0.000	0.000	2.651	1.533	2.473	0.905	0.111	0.109	263.000	0.8454
Eicosanes	0.000	0.000	0.000	2.366	1.309	2.194	0.808	0.095	0.097	275.000	0.8503
Heneicosanes	0.000	0.000	0.000	1.953	1.021	1.801	0.667	0.074	0.080	291.000	0.8552
Docosanes	0.000	0.000	0.000	1.922	0.959	1.762	0.656	0.070	0.078	305.000	0.8602
Tricosanes	0.000	0.000	0.000	1.874	0.897	1.709	0.640	0.065	0.075	318.000	0.8651
Tetracosanes	0.000	0.000	0.000	1.688	0.776	1.532	0.576	0.056	0.068	331.000	0.8691
Pentacosanes	0.000	0.000	0.000	1.593	0.703	1.439	0.544	0.051	0.064	345.000	0.8730
Hexacosanes	0.000	0.000	0.000	1.262	0.535	1.135	0.431	0.039	0.050	359.000	0.8769
Heptacosanes	0.000	0.000	0.000	1.492	0.607	1.336	0.509	0.044	0.059	374.000	0.8809
Octacosanes	0.000	0.000	0.000	1.322	0.518	1.180	0.451	0.038	0.052	388.000	0.8839
Nonacosanes	0.000	0.000	0.000	1.253	0.474	1.114	0.428	0.034	0.049	402.000	0.8868
Triacotanes	0.000	0.000	0.000	1.037	0.379	0.919	0.354	0.028	0.041	416.000	0.8898
Hentriacontanes Plus	0.000	0.000	0.000	15.788	4.251	13.499	5.390	0.309	0.596	565.000	0.9225
TOTALS	100.000	100.000	7.592	100.000	100.000	100.000	100.000	100.000	11.427	---	---

SEPARATOR OIL PLUS FRACTION CHARACTERISTICS				
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole	
	°API	**		
C <sub>7+</sub>	39.3825	0.8281	190.456	
C <sub>11+</sub>	34.5241	0.8523	265.265	
C <sub>20+</sub>	26.892	0.8934	410.693	
C <sub>31+</sub>	21.888	0.9225	565.000	

TOTAL SAMPLE CHARACTERISTICS						
COMPONENT	Specific Gravity		Molecular Weight lb/lb-mole	Vapor Volume Scf/Gal	GHV	
	°API	**			Dry ***	Saturated ***
Separator Gas	N/A	0.7979	23.007	131.718	1,348	1325
Separator HC Liquid	47.903	0.7887	152.142	16.453	N/A	126,787
Wellstream	N/A	1.1185	32.394	87.510	N/A	N/A

\* GPM (gallons per Mscf) determined at 14.65 psia and 60°F

\*\* Gas specific gravity determined relative to air (SG=1.000).  
HC Liquid and wellstream specific gravity determined relative to water (SG=1.000).  
SG values determined mathematically using the compositional analysis.

\*\*\* Gross Heating Value units for gas (real basis) and HC liquid are BTU/Scf and BTU/Gal, respectively.

**NOTE:** MW and SG values for SCN groups C<sub>6</sub> through C<sub>30</sub> taken from

"Katz, D. L., and Firoozabadi, A.: "Predicting Phase Behavior of Condensate/Crude

"Oil Systems Using Methane Interaction Coefficients; J. Pet. Tech., 228,(Nov.1978) 1649-1655.





## HOFFMAN PLOT

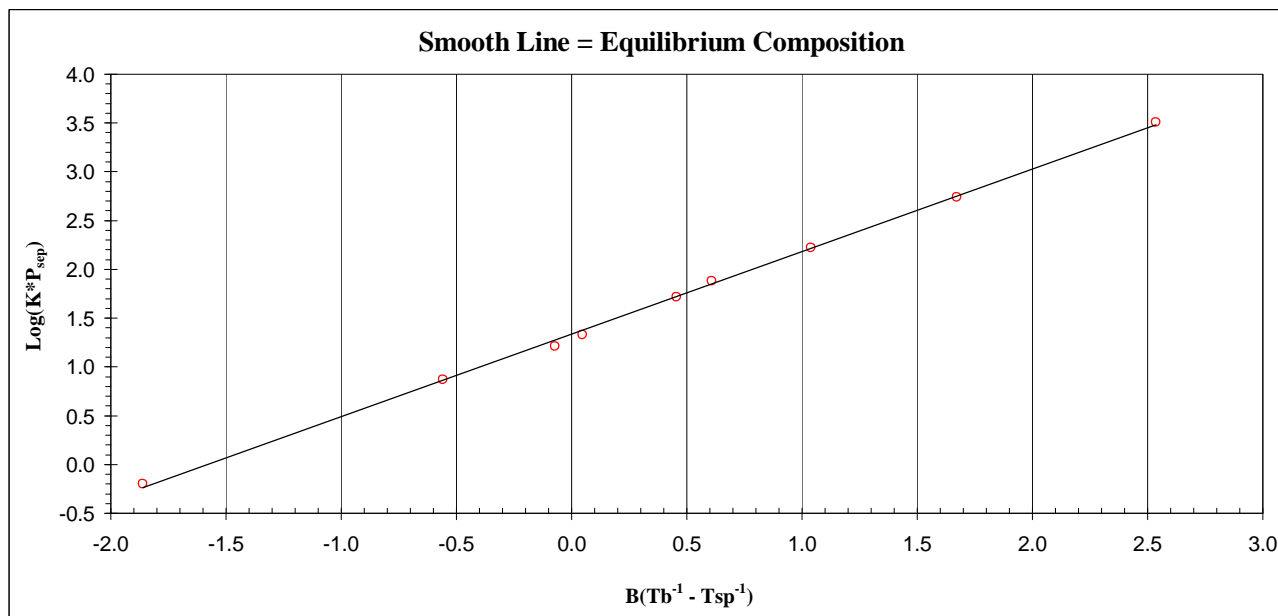
### EQUILIBRIUM CHECK of SEPARATOR HC LIQUID and GAS COMPOSITIONAL ANALYSES

Separator Pressure = 110 psia

Separator Temperature = 88 °F

Components	Gas (X)	HC Liquid (Y)	Equil. Ratio (K=Y/X)	K*Psep (psiA)	Normal BP (NBP) °R	$T_{NBP}^{-1} - T_{SEP}^{-1}$	Critical Pressure (Pc) psiA	Critical Temperature (Tc) °R	B-Factor	Graph Results	
	Mole %	Mole %								B(1/Tb-1/Tsp)	Log(K*Psep)
N2	0.000	0.000									
CO2	1.094	0.023	48.459	5313.57	139	0.005353	493	227	551	2.947	3.725
C1	0.796	0.065	12.150	1332.24	350	0.001028	1071	548	1811	1.862	3.125
C2	71.217	2.437	29.223	3204.35	201	0.003149	668	343	805	2.536	3.506
C3	14.755	2.926	5.043	553.01	332	0.001184	708	550	1413	1.673	2.743
C4	7.128	4.670	1.526	167.35	416	0.000578	616	666	1799	1.040	2.224
IC4	0.743	1.070	0.694	76.13	471	0.000299	529	735	2038	0.609	1.882
NC4	2.297	4.861	0.473	51.81	491	0.000211	551	765	2158	0.456	1.714
IC5	0.495	2.548	0.194	21.30	542	0.000020	490	829	2383	0.048	1.328
NC5	0.650	4.377	0.148	16.28	557	-0.000029	489	845	2483	-0.072	1.212
C6	0.416	6.100	0.068	7.48	615	-0.000201	437	913	2784	-0.560	0.874
C7+	0.408	70.923	0.006	0.63	763	-0.000516	332	1070	3607	-1.860	-0.200
Total	100.000	100.000									

( Note: C7+ Critical Properties as C9. The C6 composition includes iso-hexanes. )





**TABLE 2**  
**FLASH LIBERATION OF 1st-STAGE SEPARATOR HC LIQUID**

SEPARATOR CONDITIONS and FLUID PROPERTIES						
Conditions	Pressure psia	Temperature °F	GLR (1)	Separator HC Liquid Volume Factor (2)	HC Liquid Specific Gravity (3)	Gas Specific Gravity (4)
1st Stage Separator	110	88	N/A	1.0409	0.7821	0.7980
2nd Stage Separator	55	88	37	N/A	N/A	1.0780
Ambient Lab Conditions	14.84	70	37	1.0048	0.7994	1.2734
Standard Conditions	14.65	60	0	1.0000	0.8033	1.2734
TOTALS	-----	-----	74		-----	-----

Stock Tank HC Liquid Gravity: 44.65 °API at 60 °F

- (1) Gas-HC Liquid Ratio (GLR) is the cubic feet of gas at standard conditions per barrel of HC liquid at standard conditions.
- (2) Barrels of HC liquid at indicated separator conditions per barrel of HC liquid at standard conditions.
- (3) Water = 1.000
- (4) Air = 1.000
- (5) Stock Tank = Standard Conditions



**TABLE 3**  
**PRESSURE-VOLUME RELATION**  
**OF**  
**A 8628 Scf/Sep Bbl RESERVOIR FLUID AT 165 °F**  
**(Constant Composition Expansion)**

Pressure, (psia)	Relative Volume	Density, (g/cc)	Y-Function (1)	Retrograde HC Liquid Volume		Gas Deviation Factor, Z	Gas Expansion Factor, (4)
				% of HC Pore Volume (2)	Bbls / MMscf (3)		
9015	0.98538	0.45595	N/A	N/A	N/A	1.53889	1.85493
8797	0.99072	0.45350	N/A	N/A	N/A	1.50981	1.84495
8701	0.99300	0.45245	N/A	N/A	N/A	1.49677	1.84070
8420	Psat 1.00000	0.44929	N/A	0.00%	0.000	1.45864	1.82782
8055	1.00962	N/A	4.71191	0.64%	3.479	N/A	N/A
7699	1.01942	N/A	4.82128	0.93%	5.089	N/A	N/A
7295	1.03280	N/A	4.70144	1.22%	6.647	N/A	N/A
6906	1.04611	N/A	4.75501	1.72%	9.374	N/A	N/A
6201	1.07603	N/A	4.70671	3.71%	20.227	N/A	N/A
5894	1.09198	N/A	4.65955	5.07%	27.654	N/A	N/A
5611	1.10855	N/A	4.61217	6.57%	35.859	N/A	N/A
5112	1.14345	N/A	4.51136	9.66%	52.685	N/A	N/A
4815	Pres 1.16876	N/A	4.43688	12.00%	65.446	N/A	N/A
4339	1.21920	N/A	4.29120	14.92%	81.377	N/A	N/A
3792	1.30090	N/A	4.05649	18.44%	100.566	N/A	N/A
3397	1.38664	N/A	3.82477	20.66%	112.666	N/A	N/A
3097	1.47486	N/A	3.61990	22.11%	120.585	N/A	N/A
2762	1.61026	N/A	3.35719	23.47%	127.985	N/A	N/A
2373	1.84041	N/A	3.03259	24.65%	134.451	N/A	N/A
1896	2.30870	N/A	2.62975	25.45%	138.787	N/A	N/A
1386	3.25695	N/A	2.24919	25.18%	137.333	N/A	N/A
1103	4.21120	N/A	2.06647	24.26%	132.296	N/A	N/A

(1) Y - Function = Dimensionless Compressibility =  $(P_{sat} - P_i) * [P_i * (RV_i - 1)]^{-1}$

(2) Retrograde HC liquid volume at the indicated pressure and reservoir temperature as a percent of the hydrocarbon pore volume at the dew point pressure and reservoir temperature.

(3) Retrograde HC liquid volume at the indicated pressure and reservoir temperature (Bbls) per volume of gas (MMscf) at the dew point pressure and reservoir temperature.

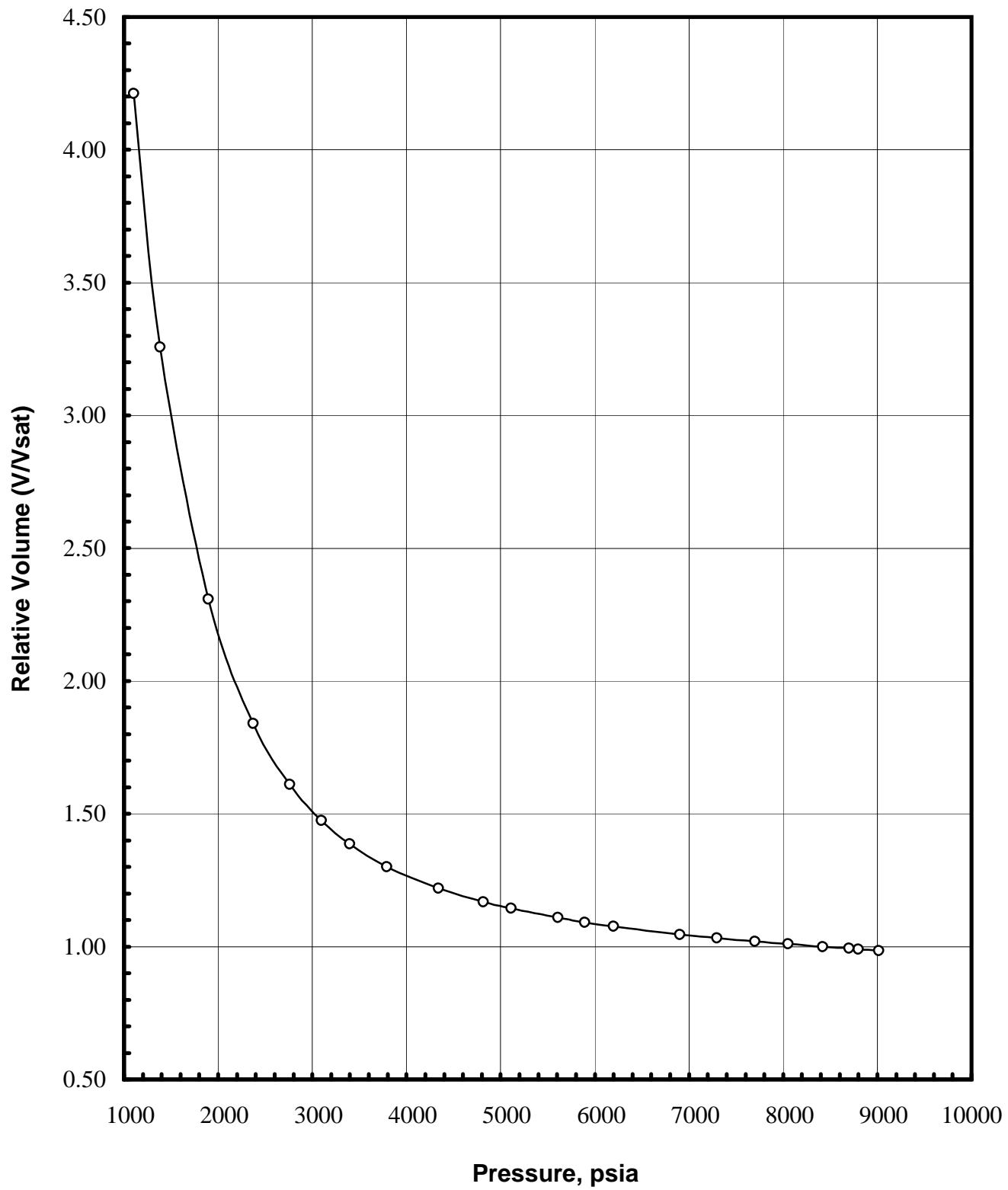
(4) Gas Expansion Factor = the volume of surface gas at standard conditions (Mscf) produced from one barrel of undersaturated gas at the indicated pressure and reservoir temperature.

Relative Volume = volume at indicated pressure per volume at the saturation pressure.

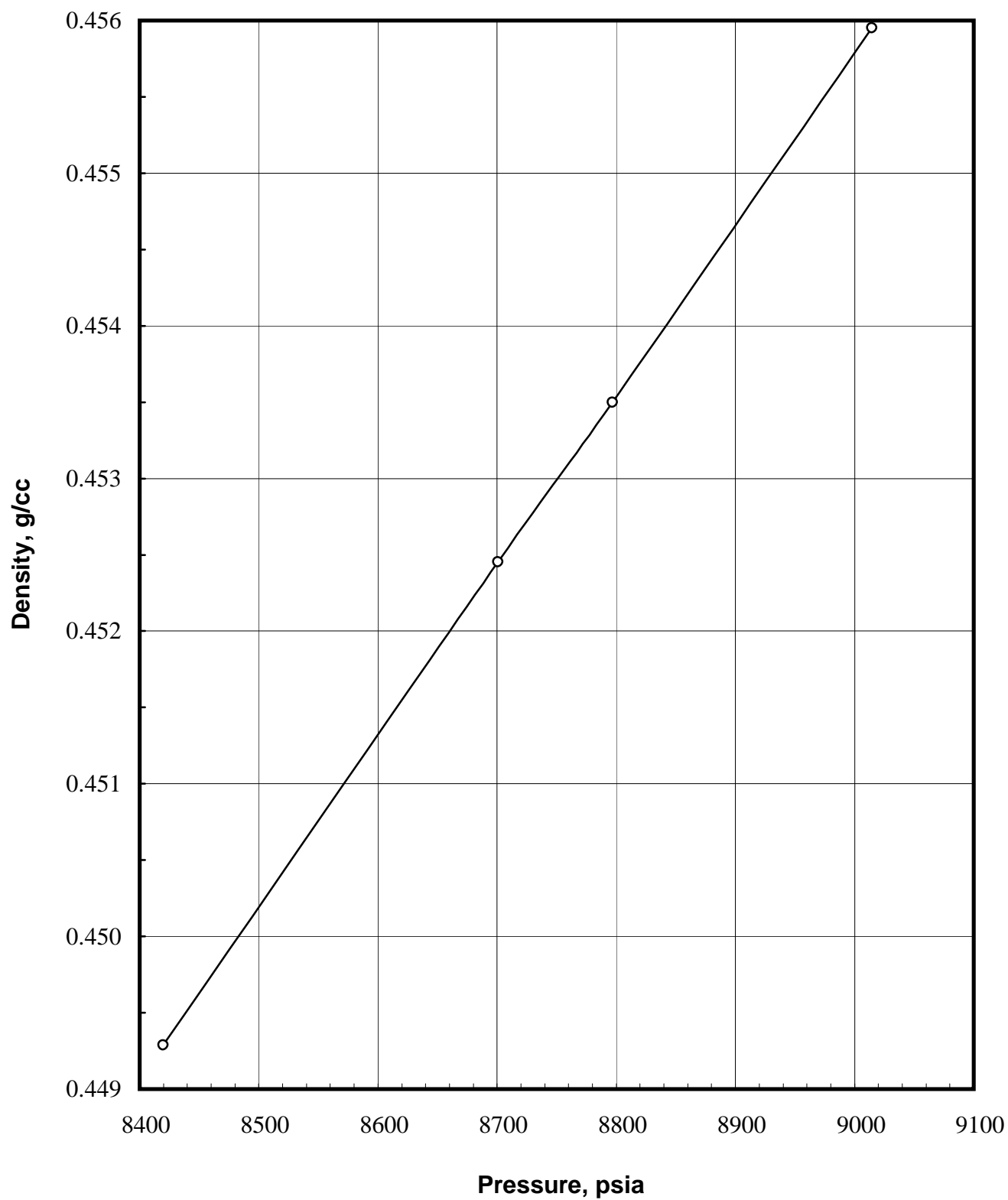
Psat = Saturation (Retrograde Dew Point) pressure at reservoir temperature.

Pres = Current static reservoir pressure.

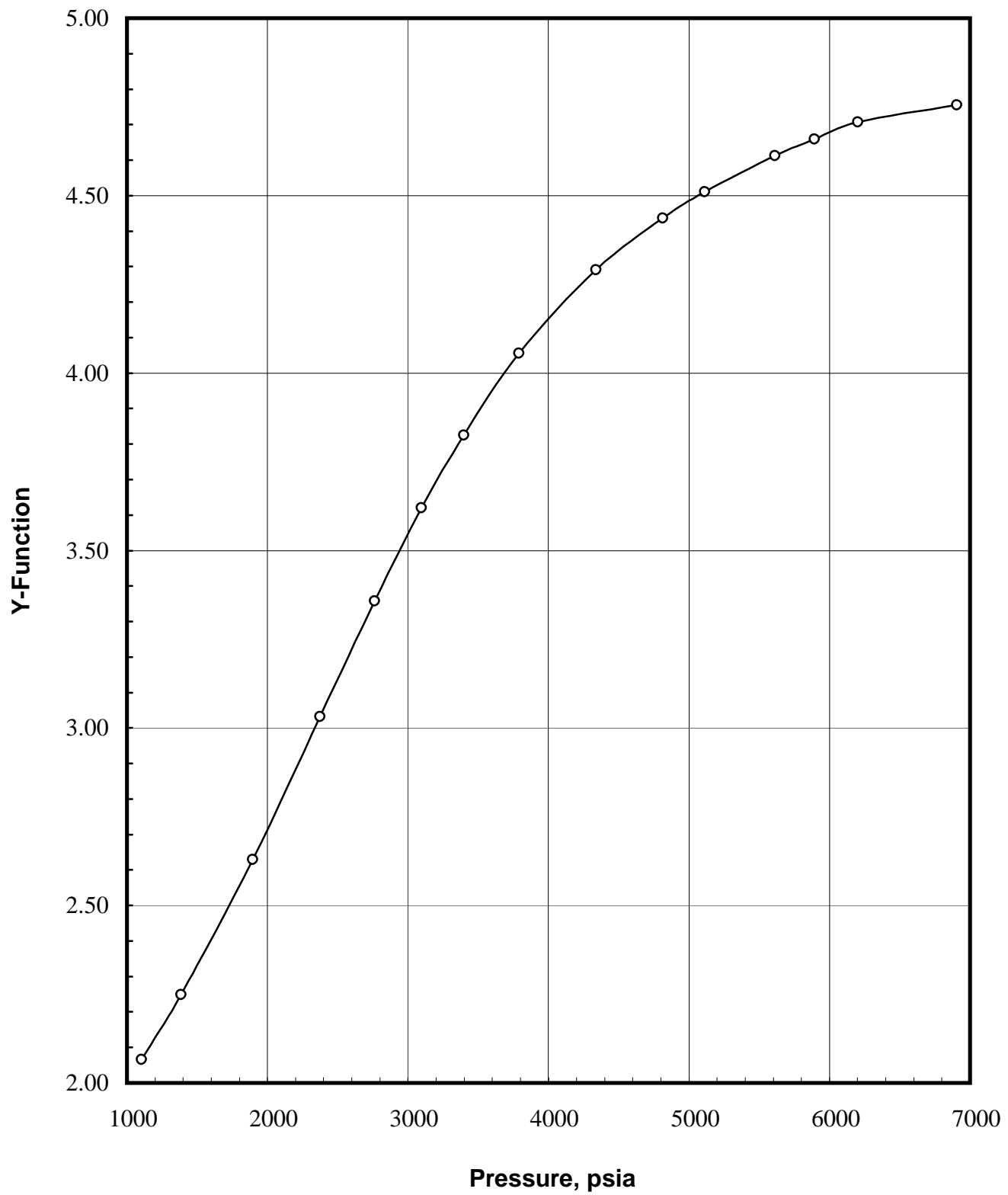
**FIGURE 1**  
**Relative Volume vs Pressure**



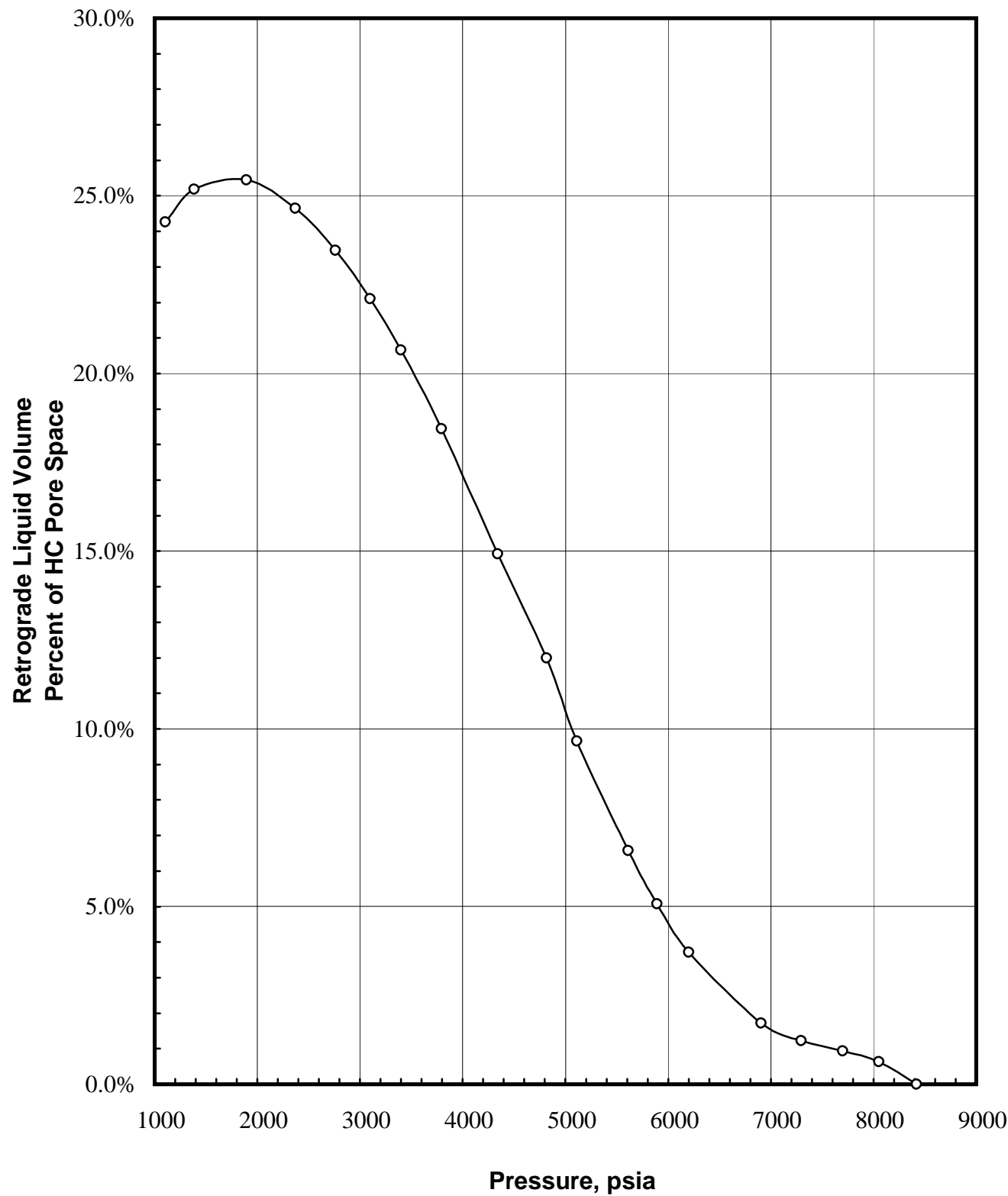
**FIGURE 2**  
**Density vs Pressure**



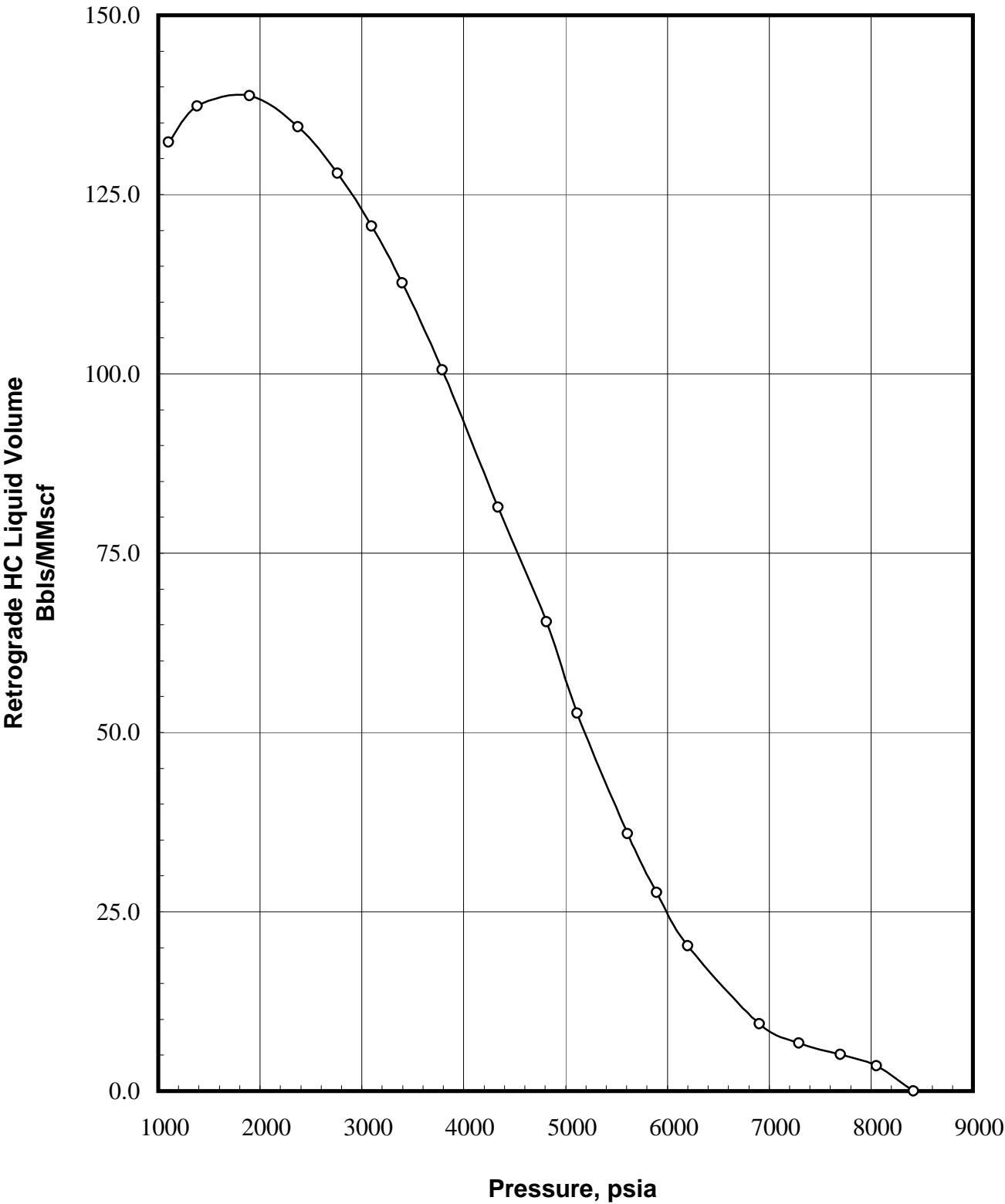
**FIGURE 3**  
**Y-Function vs Pressure**



**FIGURE 4**  
**Retrograde HC Liquid Volume vs Pressure**

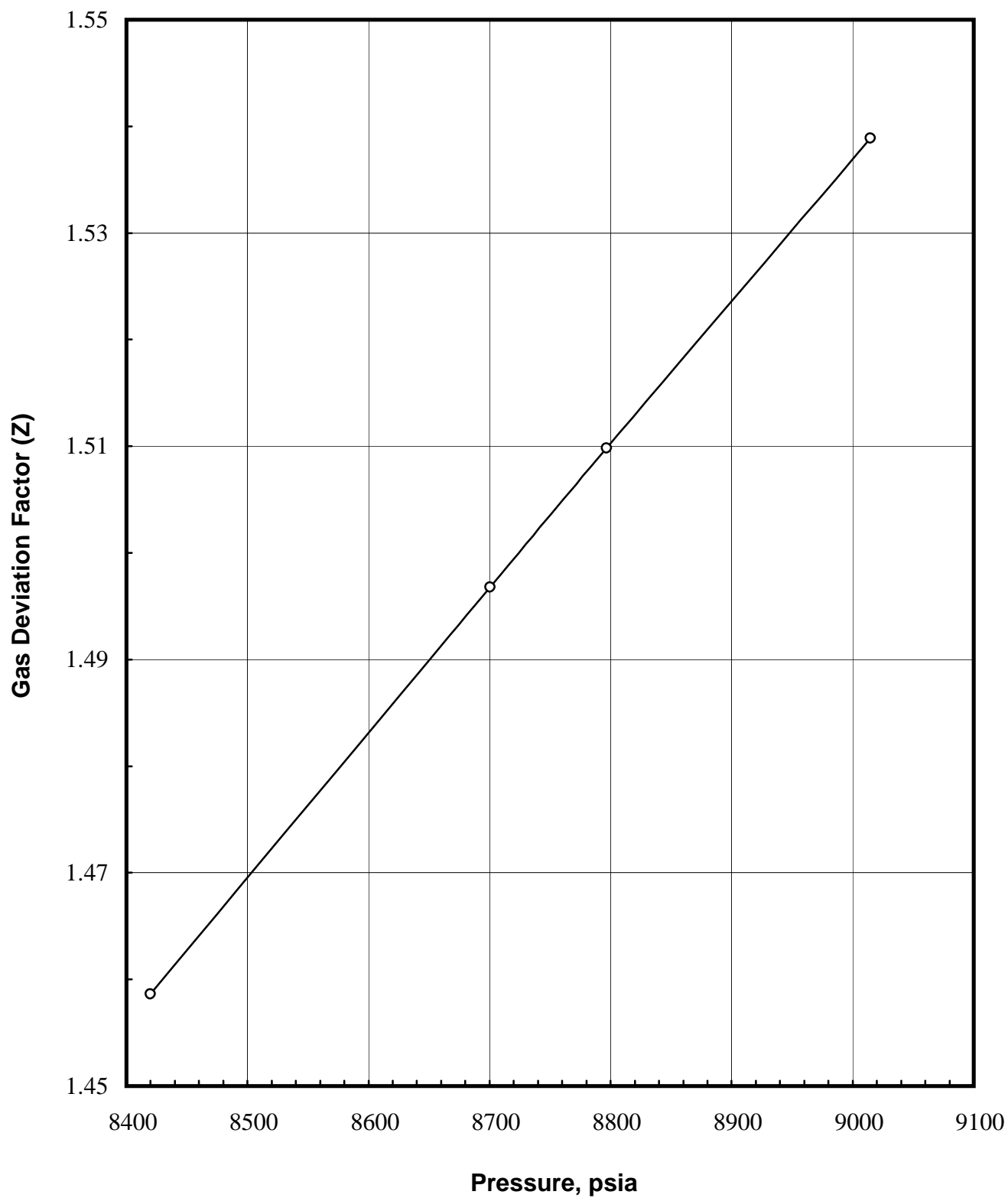


**FIGURE 5**  
**Retrograde HC Liquid Volume vs Pressure**

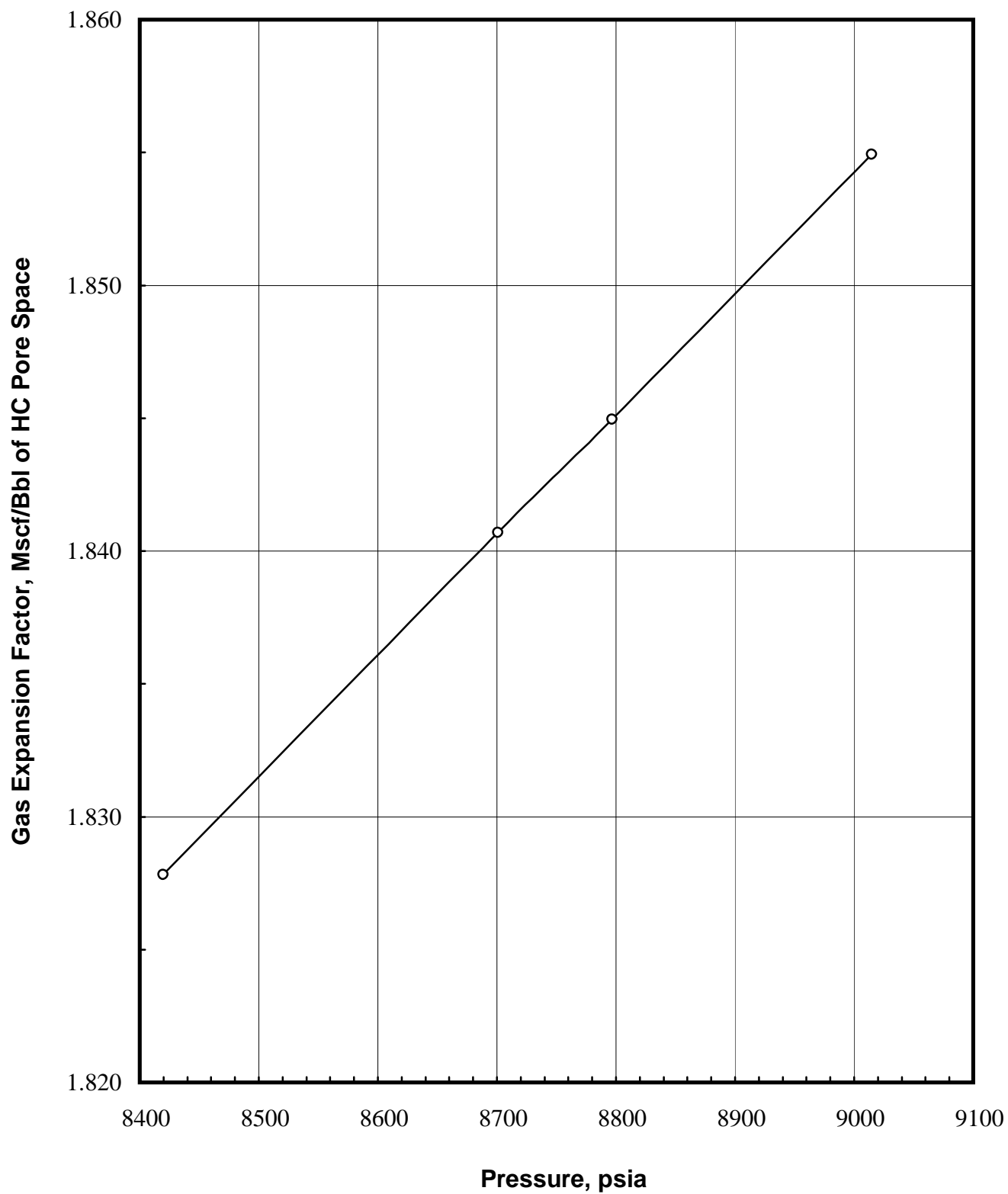




**FIGURE 6**  
**Gas Deviation Factor (Z) vs Pressure**



**FIGURE 7**  
**Gas Expansion Factor vs Pressure**



# APPENDIX



**FESCO, Ltd.**  
**1100 FESCO Ave. - Alice, Texas 78332**

For: Elevation Resources LLC  
200 N. Loraine, Suite 1010  
Midland, Texas 79701

**REPORT OF ASTM D-86 DISTILLATION**

**Oil/Condensate Sample:** University 1-26 Unit No. 5H

**Date Sampled:** 9/13/2017

**API Gravity @ 60 °F:** 44.6°

**Color:** Dark Straw

**Observed Initial Boiling Point:** 94 °F

Percent Recovered	Temperature °F
10	205
20	256
30	309
40	377
50	462
60	543
70	637
80	721
90	---
95	---
End Point	726
Recovery:	81.9 %
Residue:	16.3 %
Loss:	1.8 %
Totals:	100.0 %

**Remark:** Thermal Decomposition @ 726 deg F and 81.9% recovery.

Certified: FESCO, Ltd. - Alice, Texas

David Dannhaus (361) 661-7015

# CERTIFICATE OF COMPLIANCE AND TRANSPORTATION AUTHORITY

# P-4

This facsimile P-4 was generated electronically from data submitted to the RRC.

A certification of the automated data is available in the RRC's Austin office.

Tracking No.: 181945

1. Field name exactly as shown on proration schedule <b>EMMA (DEVONIAN)</b>		2. Lease name as shown on proration schedule <b>UNIVERSITY 1-26 UNIT</b>				
3. Current operator name exactly as shown on P-5 Organization Report <b>ELEVATION RESOURCES LLC</b>		4. Operator P-5 no. <b>247756</b>	5. Oil Lse/Gas ID no <b>283482</b>	6. County <b>ANDREWS</b>	7. RRC district <b>08</b>	
8. Operator address including city, state, and zip code <b>200 N LORAIN STE 1010 MIDLAND, TX 79701</b>		9. Well no(s) (see instruction E) <b>5H</b>				
12. Purpose of Filing. (Complete section a or b below.) (See instructions B and G) <b>a. Change of:</b> <input type="checkbox"/> operator <input type="checkbox"/> oil or condensate gatherer <input type="checkbox"/> gas gatherer <input type="checkbox"/> gas purchaser <input type="checkbox"/> gas purchaser system code <input type="checkbox"/> field name from _____ <input type="checkbox"/> lease name from _____ --- OR --- <b>b. New RRC Number for:</b> <input type="checkbox"/> oil lease <input checked="" type="checkbox"/> gas well <b>Due to:</b> <input type="checkbox"/> new completion or recompletion <input checked="" type="checkbox"/> reclass oil to gas <input type="checkbox"/> reclass gas to oil <input type="checkbox"/> other well (specify) _____ <input type="checkbox"/> consolidation, unitization, or subdivision (oil lease only)		10. Classification <input type="checkbox"/> Oil <input checked="" type="checkbox"/> Gas <input type="checkbox"/> Other (see instruction A)		11. Effective Date <b>01/15/2017</b>		
13. Authorized GAS WELL GAS or CASINGHEAD GAS Gatherer(s) and/or Purchaser(s). (See instruction G).						
Gatherer	Purchaser	Name of GAS WELL GAS or CASINGHEAD GAS Gatherer(s) or Purchaser(s) As Indicated in Columns to the Left (Attach an additional sheet in same format if more space is needed)		Purchaser's RRC Assigned System Code	Percent of Take	Full-well stream
X	X	DCP MIDSTREAM, LP(195918)		0001	50.0	
X	X	JAMES LAKE MIDSTREAM LLC(429665)		0001	50.0	
14. Authorized OIL or CONDENSATE Gatherer(s). (See instruction G).						
Name of OIL or CONDENSATE Gatherer(s) - List Highest Volume Gatherer First (Attach an additional sheet in same format if more space is needed)						Percent of Take
SUNOCO PTNRS. MKTG.&TERMINALS LP(829626)						100.0
<b>RRC USE ONLY:</b> Reviewer's initials: _____ Approval date: _____						
<b>15. PREVIOUS OPERATOR CERTIFICATION FOR CHANGE OF OPERATOR P-4 FILING.</b> Being the PREVIOUS OPERATOR, I certify that operating responsibility for the well(s) designated in this filing, located on the subject lease has been transferred in its entirety to the above named Current Operator. I understand, as Previous Operator, that designation of the above named operator as Current Operator is not effective until this certificate is approved by the Commission.						
Name of Previous Operator _____ Name (print) _____ Title _____				Signature <input type="checkbox"/> <b>Authorized Employee of previous operator</b> <input type="checkbox"/> <b>Authorized agent of previous operator (see instruction G)</b> _____ Date _____ Phone with area code _____		
<b>16. CURRENT OPERATOR CERTIFICATION.</b> By signing this certificate as the Current Operator, I certify that all statements on this form are true and correct and I acknowledge responsibility for the regulatory compliance of the subject lease including plugging of well(s) pursuant to Rule 14. I further acknowledge that I assume responsibility for the physical operation, control, and proper plugging of each well designated in this filing. I also acknowledge that I will remain designated as the Current Operator until a new certificate designating a new Current Operator is approved by the Commission.						
<b>ELEVATION RESOURCES LLC</b> Name (print) <b>Eng. Tech</b> Title <b>cflanagan@elevationres.com</b> E-mail Address (optional)				<b>Curtis Flanagan</b> Signature <input checked="" type="checkbox"/> <b>Authorized Employee of current operator</b> <input type="checkbox"/> <b>Authorized agent of current operator (see instruction G)</b> _____ Date <b>10/31/2017</b> Phone with area code <b>(432) 688-3380</b>		

**CERTIFICATE OF  
POOLING AUTHORITY**

Revised 05/2001

**P-12**

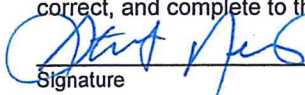
1. Field Name(s) All Fields	2. Lease/ID Number (if assigned)	3. RRC District Number 08
4. Operator Name Elevation Resources, LLC	5. Operator P-5 Number 247756	6. Well Number 5H
7. Pooled Unit Name University 1-26 Unit	8. API Number	9. Purpose of Filing <input checked="" type="checkbox"/> Drilling Permit (W-1) <input type="checkbox"/> Completion Report
10. County Andrews	11. Total acres in pooled unit 728.22	

DESCRIPTION OF INDIVIDUAL TRACTS CONTAINED WITHIN THE POOLED UNIT

TRACT/PLAT IDENTIFIER	TRACT NAME	ACRES IN TRACT (See inst. #7 below)	INDICATE UNDIVIDED INTERESTS	
			UNLEASED	NON-POOLED
*1	Tract 1	303.37	<input type="checkbox"/>	<input type="checkbox"/>
2	Tract 2	181.97	<input type="checkbox"/>	<input type="checkbox"/>
3	Tract 3	242.88	<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>

CERTIFICATION:

I declare under penalties prescribed pursuant to the Sec. 91.143, Texas Natural Resources Code, that I am authorized to make the foregoing statements and that the information provided by me or under my direction on this Certificate of Pooling Authority is true, correct, and complete to the best of my knowledge.



Signature

Stewart Newton

Print Name

Regulatory Consultant

stewart.newton@pghengineers.com

04/13/2015

(512) 480-8800

Title

E-mail (if available)

Date

Phone

INSTRUCTIONS — Reference: Statewide Rules 31, 38 and 40

- When two or more tracts are pooled to form a unit to obtain a drilling permit, file completion paperwork, or reform a pooled unit pursuant to Rule 38(d)(3) the operator must file an original Certificate of Pooling Authority and certified plat.
- The certified plat shall designate each tract with an outline and a tract identifier. The tract identifier on the plat shall correspond to the tract identifier and associated information listed on the Certificate.
- If within an individual tract, a non-pooled and/or unleased interest exists, indicate by checking the appropriate box.
- If the Purpose of Filing is to obtain a drilling permit, in box #1 list all applicable fields separately or enter "All Fields" if the Certificate pertains to all fields requested on Form W-1.
- If the Purpose of Filing is to file completion paperwork, enter the applicable field name in box #1 for the completion.
- Identify the drill site tract with an \* to the left of the tract identifier.
- The total number of acres in the pooled unit in #11 should equal the total of all acres in the individual tracts listed.

Date: mo. day yr.



Groundwater  
Advisory Unit

GROUNDWATER PROTECTION DETERMINATION

Form GW-2

Date **March 27, 2015**

GAU File No.: **17249**

API Number **00300000**

Attention: **STEWART NEWTON**

RRC Lease No. **000000**

SC\_247756\_00300000\_000000\_17249.pdf

ELEVATION RESOURCES LLC  
200 N LORAIN  
STE 1010  
MIDLAND TX 79701

--Measured--

2187 ft FEL

300 ft FNL

MRL:SECTION

Digital Map Location:

X-coord/Long **446947**

Y-coord/Lat **225263**

Datum **27** Zone **NC**

P-5# 247756

County **ANDREWS**

Lease & Well No. **UNIVERSITY 1-26 UNIT #3H**

Purpose **ND**

Location **SUR-UNIVERSITY LAND, BLK-1, SEC-26, --[TD=12000], [RRC 08],**

To protect usable-quality groundwater at this location, the Groundwater Advisory Unit of the Railroad Commission of Texas recommends:

The interval from the land surface to a depth of 250 feet and the ZN from 1275 feet to 1575 feet must be protected.

This recommendation is applicable to all wells drilled in this TRACT 1 OF SECTION 26 ON THIS LEASE.

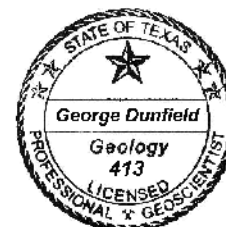
Note: Unless stated otherwise, this recommendation is intended to apply only to the subject well and not for area-wide use. This recommendation is intended for normal drilling, production, and plugging operations only. It does not apply to saltwater disposal operation into a nonproductive zone (RRC Form W-14).

If you have any questions, please contact us at 512-463-2741, [gau@rrc.state.tx.us](mailto:gau@rrc.state.tx.us), or by mail.

Sincerely,

George Dunfield, P.G.

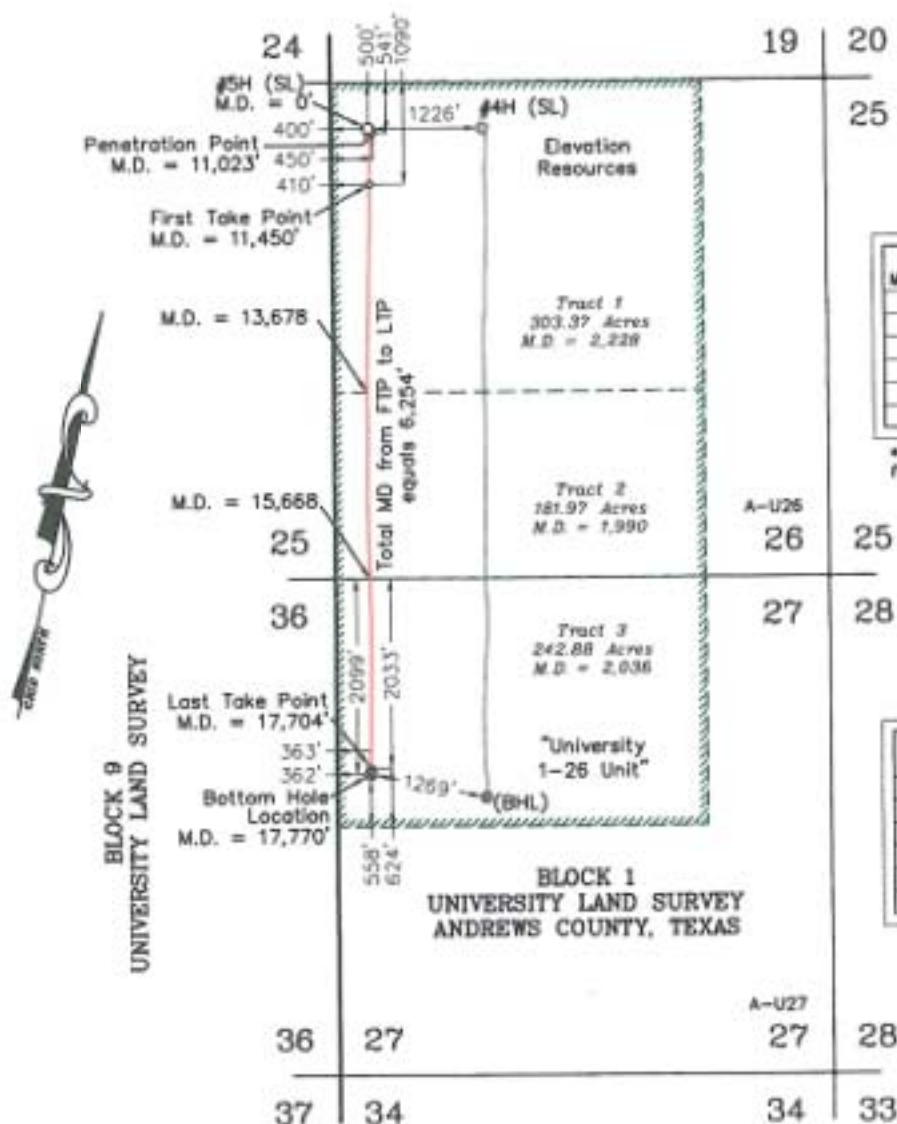
GEOLOGIST SEAL



Geologist, Groundwater Advisory Unit  
Oil & Gas Division

The seal appearing on this document was authorized by George Dunfield on 3/27/2015  
Note: Alteration of this electronic document will invalidate the digital signature.





University 1-10 Unit Measured Depth Allocation Table	
Tract 1 - 2,228 M.D.	
Tract 2 - 1,990 M.D.	
Tract 3 - 2,036 M.D.	
<b>Total - 6,254 M.D.</b>	

\*Note: Allocations are measured from First Take Point to Last Take Point

University 1-26 Unit Acreage Allocation Table	
Tract 1 - 303.37 Acres	
Tract 2 - 181.97 Acres	
Tract 3 - 242.88 Acres	
<b>Total - 728.22 Acres</b>	

	State Plane Coordinate		Geodetic (D.M.S.)		Geodetic (D.D.)	
Surface Location	X = 444,329.80	Y = 224,479.38	Lat = 32°10'52.70" N	Long = 102°31'47.37" W	Lat = 32.18130583° N	Long = 102.52982580° W
Penetration Point	X = 444,387.93	Y = 224,449.94	Lat = 32°10'52.44" N	Long = 102°31'46.68" W	Lat = 32.18123265° N	Long = 102.52963359° W
First Take Point	X = 444,467.98	Y = 223,905.55	Lat = 32°10'47.09" N	Long = 102°31'45.45" W	Lat = 32.17974849° N	Long = 102.52929098° W
Last Take Point	X = 445,779.11	Y = 217,795.38	Lat = 32°09'47.32" N	Long = 102°31'26.81" W	Lat = 32.16314445° N	Long = 102.52411429° W
Bottom Hole Location	X = 445,791.88	Y = 217,730.78	Lat = 32°09'46.69" N	Long = 102°31'26.63" W	Lat = 32.16296877° N	Long = 102.52406308° W

The University 1-26 Unit #5H is located approximately 10 miles South-Southeast of Andrews, Texas.

Downhole Path based on Survey Report received from Elevation Resources on February 8, 2017.

Prepared From Survey Dated: November 3, 2014



#### Legend

- Denotes Downhole Directional Well Path
- Denotes Proposed Well Location
- Denotes Proposed Take Points
- Denotes Proposed Bottom Hole Location
- Denotes Unit Boundary
- Denotes Tract Line

#### NOTE:

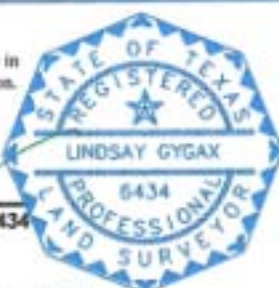
- 1) Plane Coordinates shown hereon are Lambert Grid and Conform to the "Texas Coordinate System", Texas North Central Zone, North American Datum of 1927, unless otherwise noted. Scale factor is 1.000169588.
- 2) Geodetic Coordinate shown hereon references the North American Datum of 1927, unless otherwise noted.
- 3) This plat is provided only for filing purposes with the Texas Railroad Commission and should not be construed as a boundary survey.
- 4) Measured Depth allocation is approximate and based on downhole report and take points as provided by client.

#### CERTIFICATION:

I hereby certify that this plat was made from notes taken in the field in a bona fide survey made under my supervision.

Lindsay Gygax

Texas R.P.L.S. No. 6434



**WEST COMPANY**

Land Surveyors & Civil Engineers

110 W. Louisiana Ave., Suite 110, Midland, Texas 79701  
(432) 687-0865 - FAX (432) 687-0868  
FIRM Registration Number: 100882-00



#### UNIVERSITY 1-26 UNIT #5H DOWNHOLE REPORT

Crossing Sections 26 and 27  
Block 01

All in University Lands Survey  
Andrews County, Texas

Scale: 1" = 2000'

Surveyed: 11/03/14

File: J:\2017\2014-1457-1\2014-1457-1 University 1-26 5H As-Drilled.dwg

W.O.: 2014-1457-1

Drawn By: SC